

**Wetlands for Water Management**

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# The use of aeration in VSSF to reduce land area requirements in CWs

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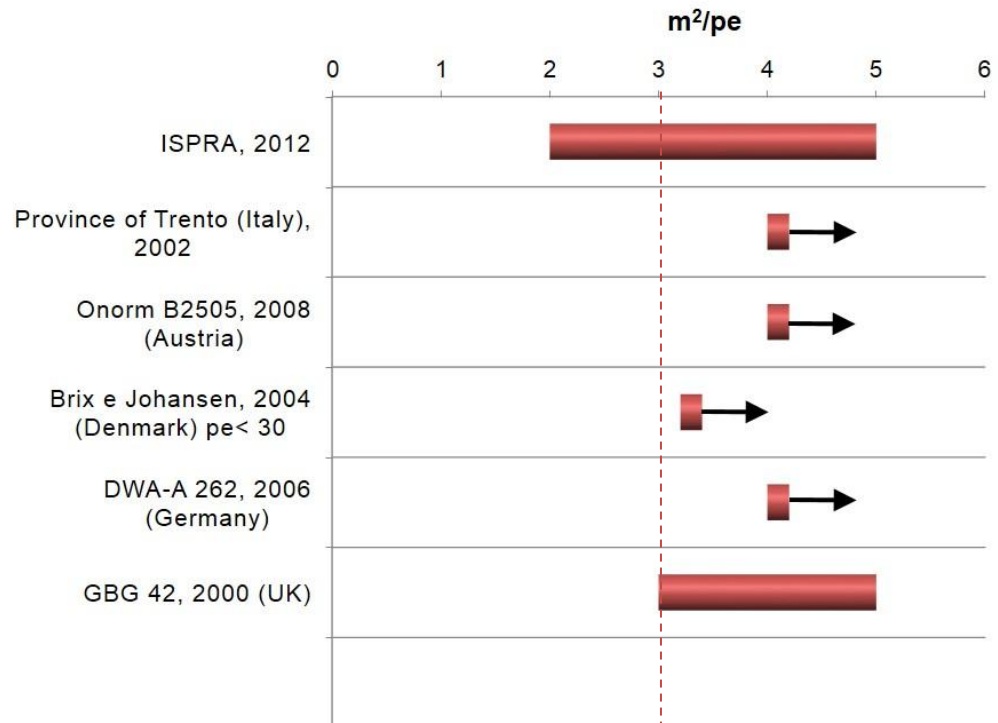
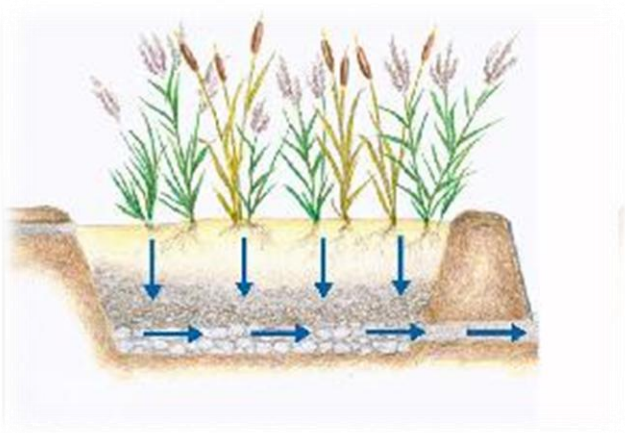
# Contents

- Mountain context
- Aerated VSSF – methods
- Results
- Conclusions

# Introduction

Constructed wetlands (CW) are known for low costs, sustainability and efficiency in the treatment of municipal wastewater.

The LAND AREA REQUIREMENT is the main barrier for the application in tourist villages and small agglomerations in the Alps region.



Vertical Sub-Surface Flow (VSSF) CWs

# Introduction

- Some efforts have been made in literature to improve the conventional CW with the aim to reduce land area requirements and enhance nitrification and nitrogen removal.

Among some techniques utilized:

- alternate feeding periods
- recirculation of the treated wastewater
- 
- **artificial aeration** in HSSF  
(conventionally oxygen-limited systems).

# Objectives

- The aim of this research was to apply innovative configurations in the VSSF to reduce land area requirements and enhance nitrification and nitrogen removal.

✓ Intermittent artificial aeration in the saturated layer.

For the reduction of land area higher hydraulic and organic loads were applied.

Innovative high load configuration was compared with a conventional CW configuration.

# Methods



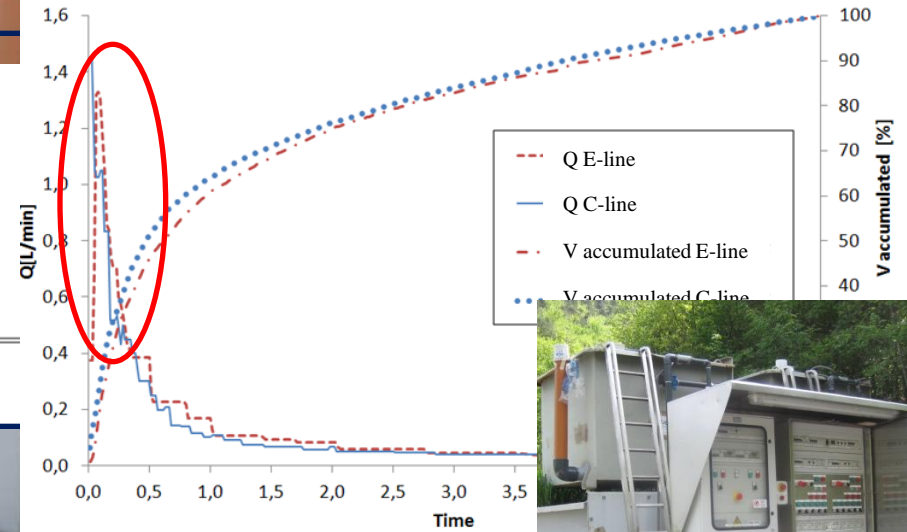
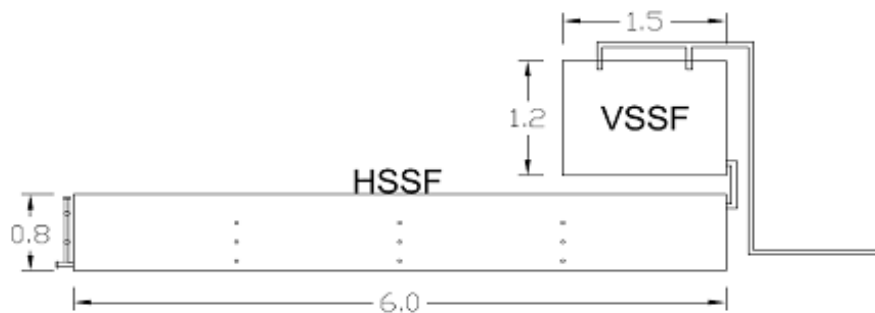
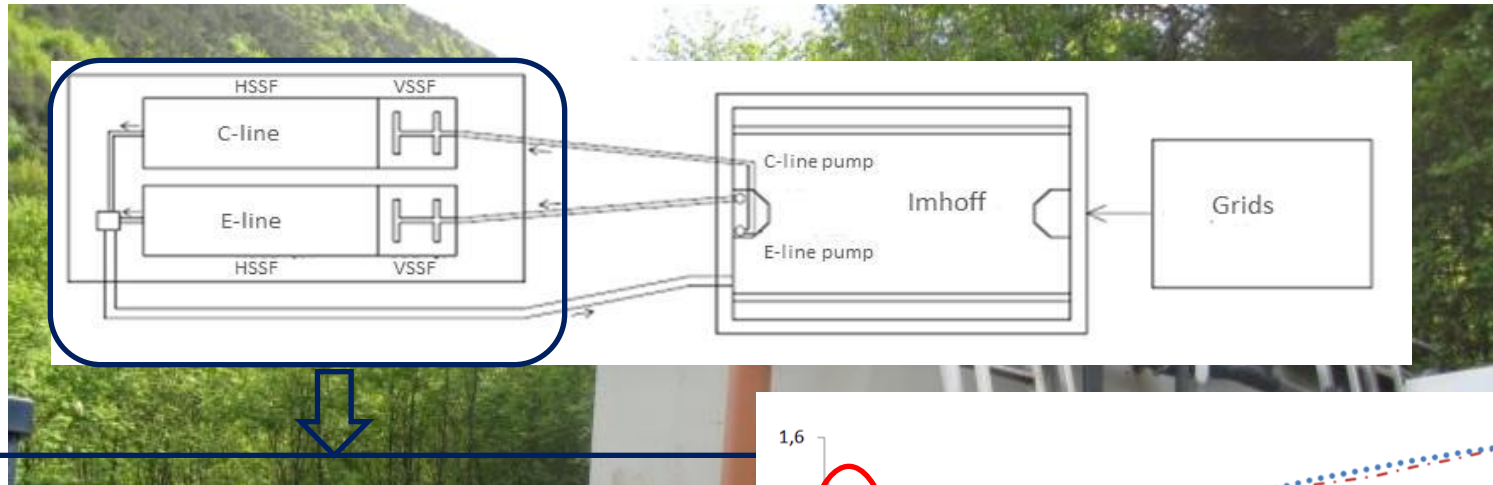
Ranzo  
Province of Trento  
Italy

Location: Alps region  
Elevation: 739 m a.s.l.

Pilot Plant



# Pilot plant



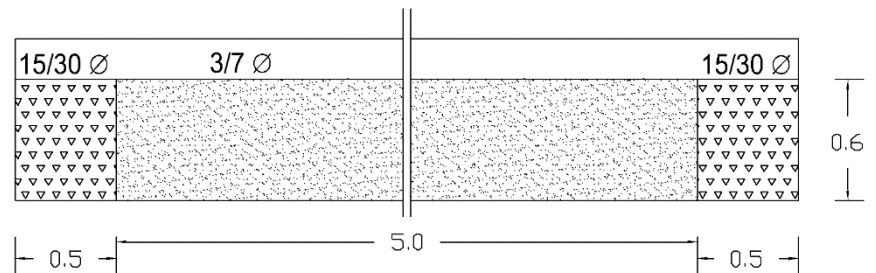
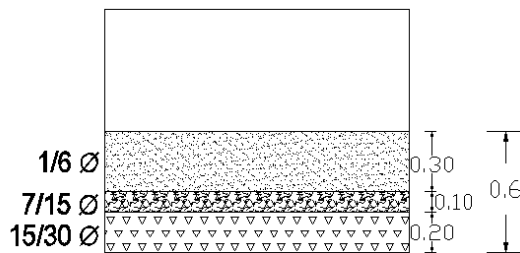
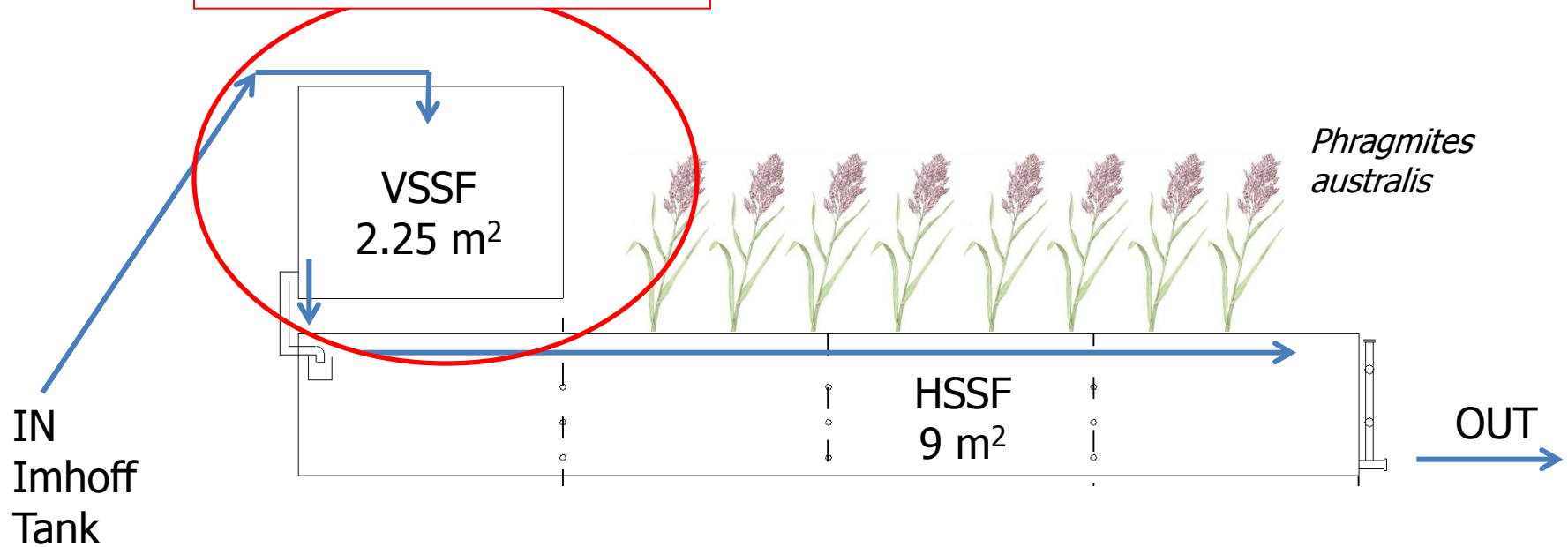
Inlet/outlet samples and Track studies:  
 COD, COD soluble, TSS,  $\text{NH}_4\text{-N}$ ,  $\text{NO}_3\text{-N}$ ,  
 $\text{NO}_2\text{-N}$ , TKN, Total P,  $\text{P-PO}_4^{3-}$  (APHA, 2005)





# Methods

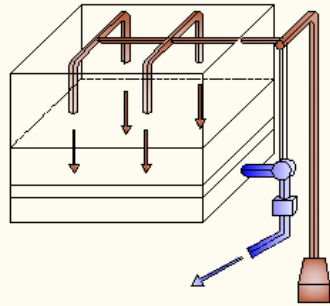
Innovative configurations





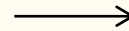
# Methods

## Configurations tested



FEEDING AND  
FREE-DISCHARGE

Conventional down-flow  
configuration

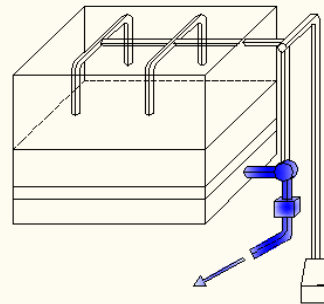
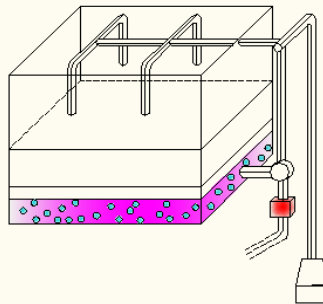
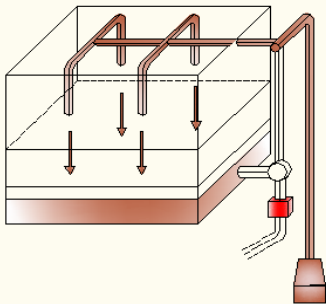


1) Low Load VSSF:  $3.2 \text{ m}^2/\text{pe}$

FEEDING

AERATION

DISCHARGE



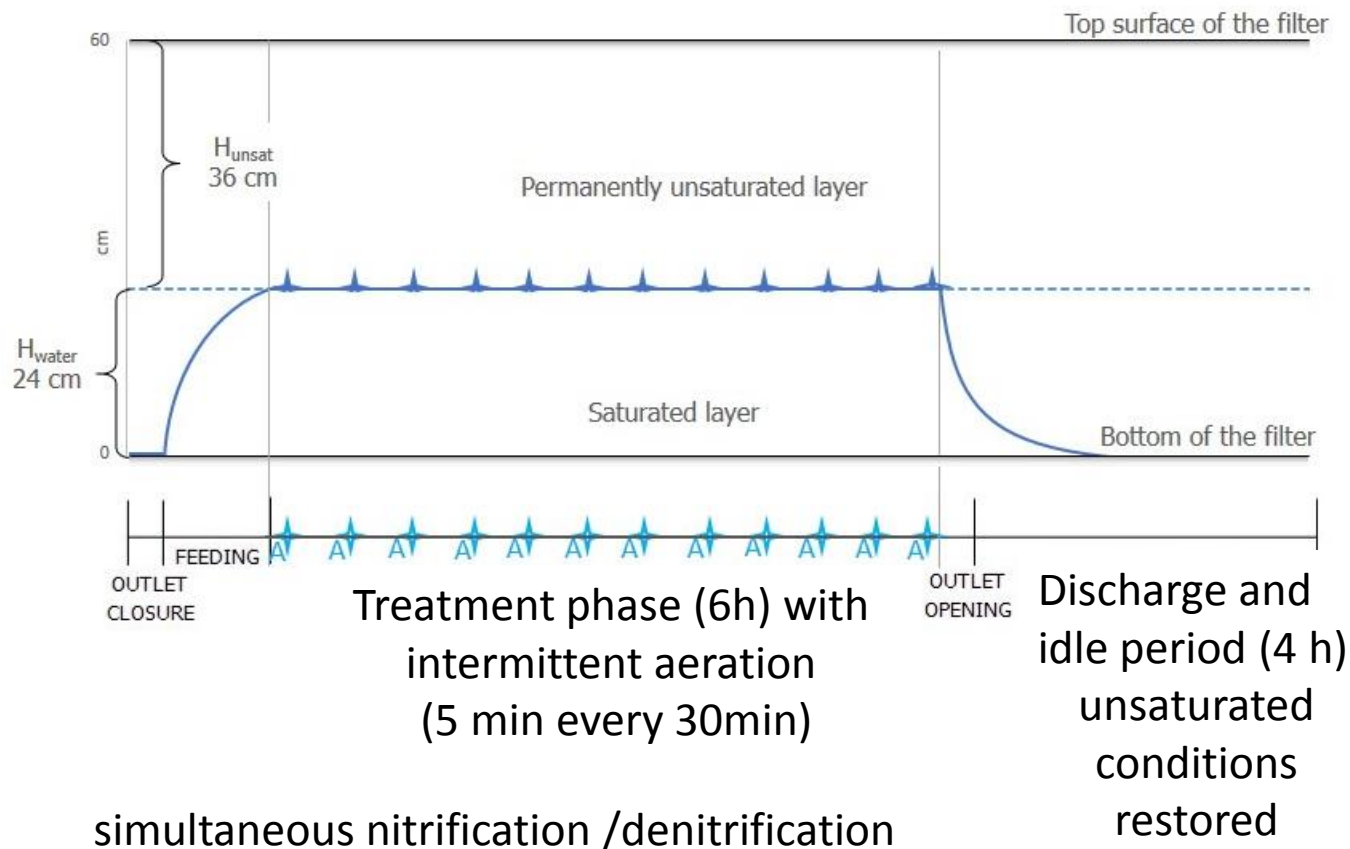
2) High Load Aerated VSSF:  
 $1.9 \text{ m}^2/\text{pe}$

Aeration:  
5 min every 30 min

Equipment: small air blower connected to perforated pipes on the bottom of the bed

# Methods

**Aerated VSSF:** Fill and drain VSSF + intermittent aeration in the saturated layer.



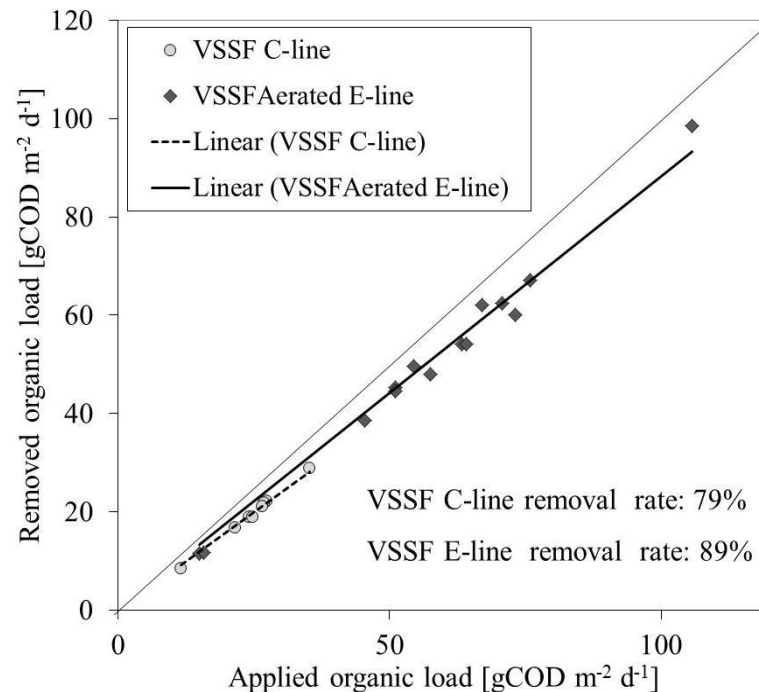
12  
Sampling  
points

# Methods

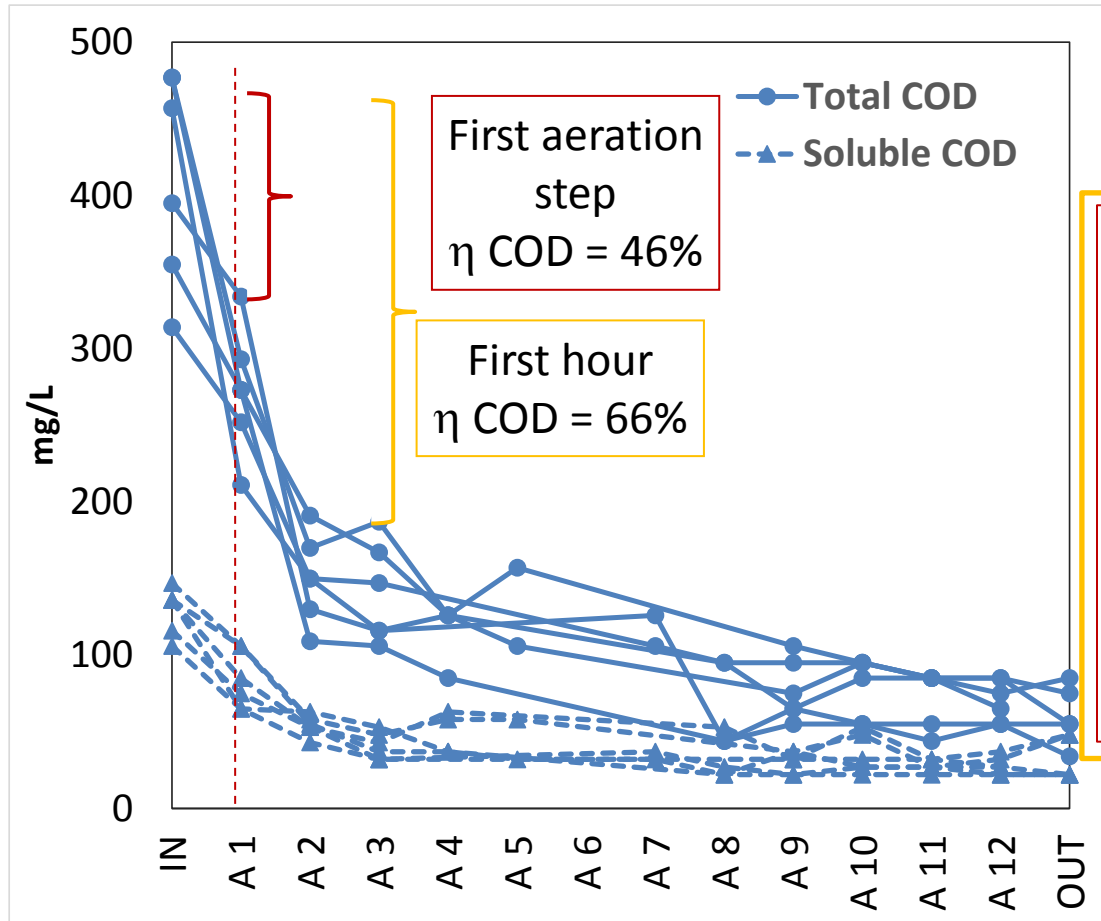
	Parameter	Units	Aerated VSSF	C-line
VSSF	Influent flow rate (hydraulic load)	L/d	304	149
	Specific hydraulic load	$L\ m^{-2}\ d^{-1}$	135	65
	Surface organic load	$gCODm^{-2}d^{-1}$	58	25
	Specific area	$m^2/PE$	1.9	4.2
	Cycles per day (feeds per day)	#/d	2.2	3.6
	Resting period (between feeds)	H	10.8	6.6
HSSF	Specific hydraulic load	$L\ m^{-2}\ d^{-1}$	34	16
	Specific area (all the bed= 9 $m^2$ )	$m^2/PE$	8.7	19.5

# Results

Parameter		Aerated VSSF	C-Line
COD	Applied COD load in VSSF [ $\text{gCOD m}^{-2} \text{d}^{-1}$ ]	57.6	24.8
	Removed COD load in VSSF [ $\text{gCOD m}^{-2} \text{d}^{-1}$ ]	50.7	19.7



# Results



First passage through the bed:

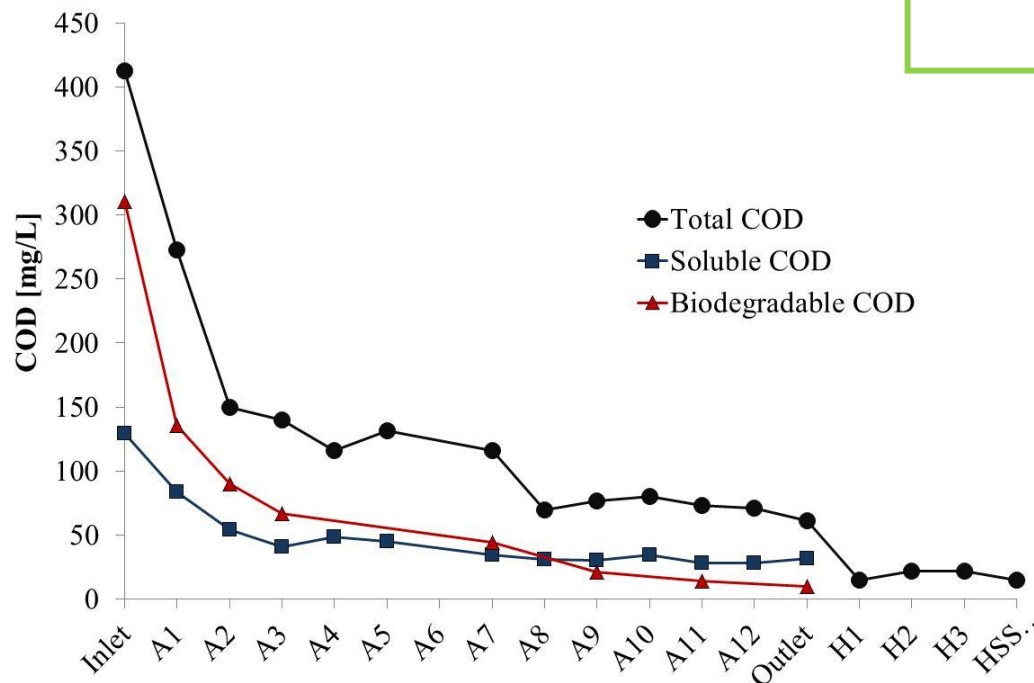
- Pore water dilution;
- Physical retention of particulated COD;
- Biological oxidation of biodegradable compounds

Time-profiles during the treatment phase in the A-VSSF: Total COD and sCOD.  
Legend: IN = influent wastewater; A1-A12 = intermittent aerations; OUT = effluent wastewater.

# Results

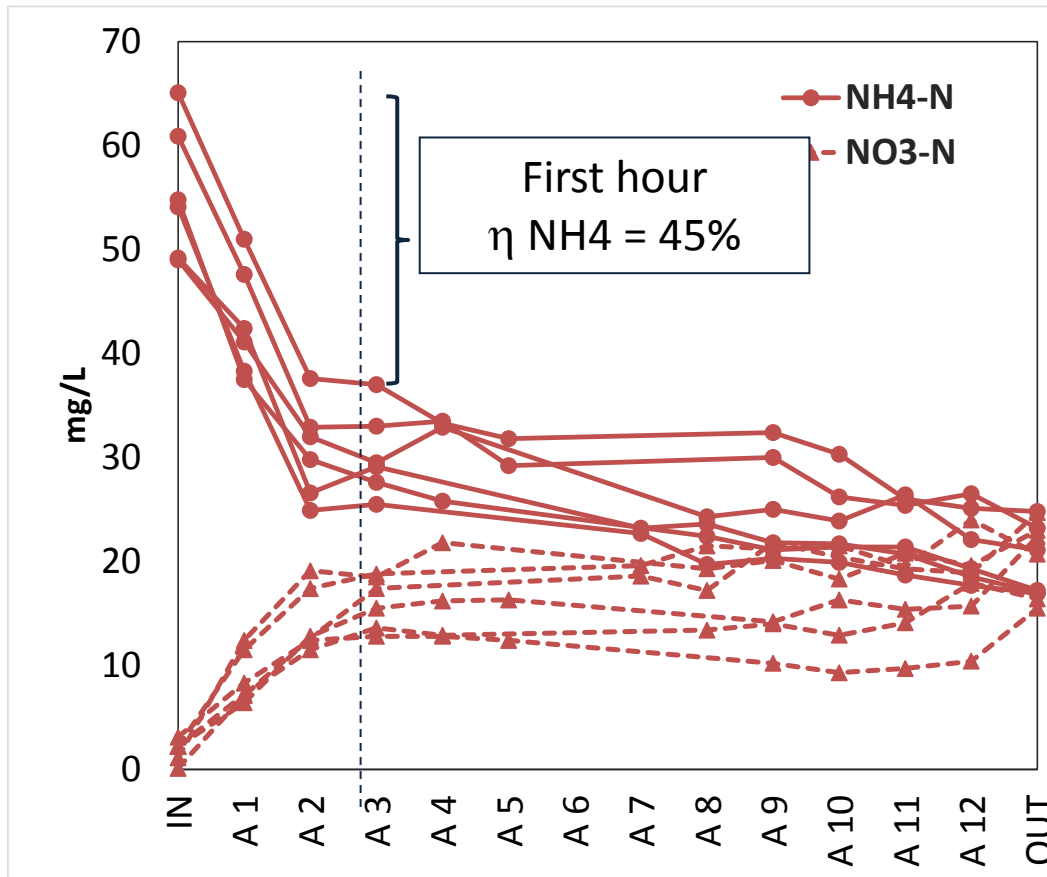
High removal efficiencies  
→ Longer HRT

COD	Aerated VSSF	C-line
VSSF Efficiency	89%	79%
VSSF Effluent	52 mg/L	105 mg/L
VSSF+HSSF Efficiency	96%	92%
VSSF+HSSF Effluent	19 mg/L	23 mg/L



Polishing function

# Results



NH<sub>4</sub>-N concentration in the bed not significantly reduced by intermittent aeration on the bottom.

Reasons: nitrifying bacteria less present or insufficient oxygen supplied by aeration.

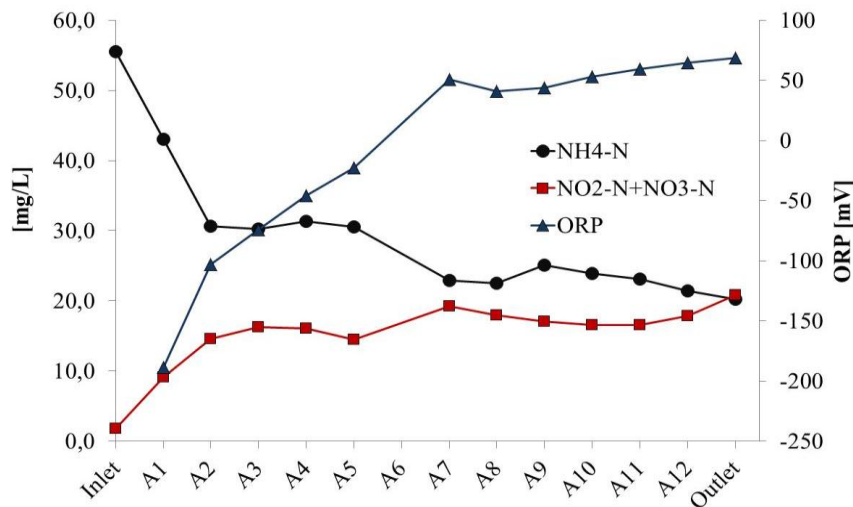
Time-profiles during the treatment phase in the A-VSSF: NH<sub>4</sub>-N and NO<sub>3</sub>-N.

Legend: IN = influent wastewater; A1-A12 = intermittent aerations; OUT = effluent wastewater.



# Results

$\text{NH}_4\text{-N}$	Aerated VSSF	C-line
VSSF Efficiency	69%	79%
VSSF Effluent	19.4 mg/L	13.2 mg/L
VSSF+HSSF Efficiency	93%	92%
VSSF+HSSF Effluent	5.7 mg/L	4.9 mg/L



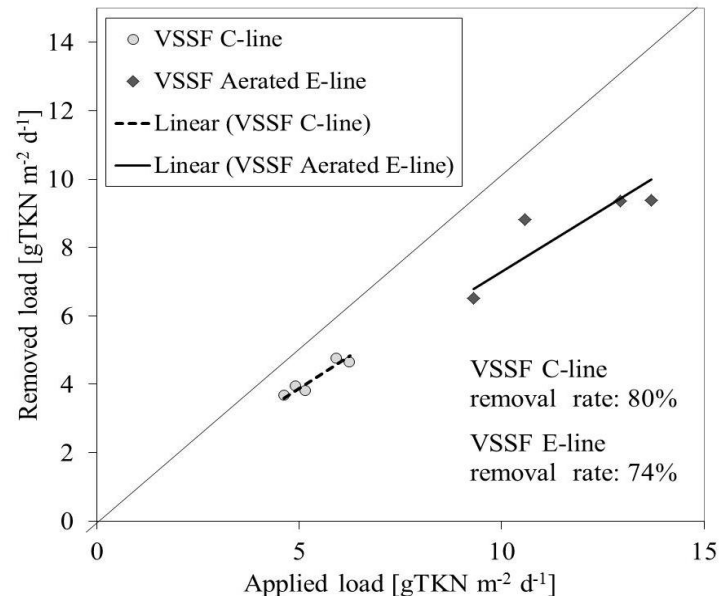
$\text{NO}_x\text{-N}$  produced +18 mgN/L  
TKN removed -59 mgN/L

Higher Denitrification  
(longer HRT + saturated  
conditions not fully  
aerobic).

$\text{NO}_3\text{-N}$	Aerated line	C-line
VSSF Effluent	20 mg/L	39 mg/L
VSSF+HSSF Effluent	12.7 mg/L	17.7 mg/L <sup>16</sup>

# Results

	Parameter	Aerated VSSF	C-Line
TKN	Applied TKN load in VSSF [ $\text{gTKN m}^{-2} \text{d}^{-1}$ ]	12.4	5.4
	Removed TKN load in VSSF [ $\text{gTKN m}^{-2} \text{d}^{-1}$ ]	9.2	4.3
Total N	Applied total N load in VSSF [ $\text{gN m}^{-2} \text{d}^{-1}$ ]	13.6	5.5
	Removed total N load in VSSF [ $\text{gN m}^{-2} \text{d}^{-1}$ ]	7.2	1.9



# Conclusions

- The high-load Aerated VSSF is a promising technique in terms of carbon and nitrogen removal.
- Aeration cannot fill all the porosity of the bed and thus the liquid volume results not entirely aerated:

heterogeneous and anoxic conditions in the granular medium allowing simultaneous NITRIFICATION and DENITRIFICATION in the saturated layers at the bottom of the bed.

- Total Nitrogen (TN) removal was benefited from the saturated bottom of VSSF CW: the availability of organic matter, the longer residence time and the creation of aerobic and anoxic zones in the bed.

# Conclusions

Advantage	Drawback
Land area reduction: from the 4m <sup>2</sup> /PE suggested by the national guidelines to 1.9 m <sup>2</sup> /PE	Slightly complex system: aeration pipes, small blower and automated valve.

Aerated VSSF can be used as a permanent solution for the wastewater treatment of small communities, or as an additional one to be used during peak seasons, in order to guarantee the removal of extra-loads.



# Acknowledgment:



ISAC - Improving Skills  
Across Continents



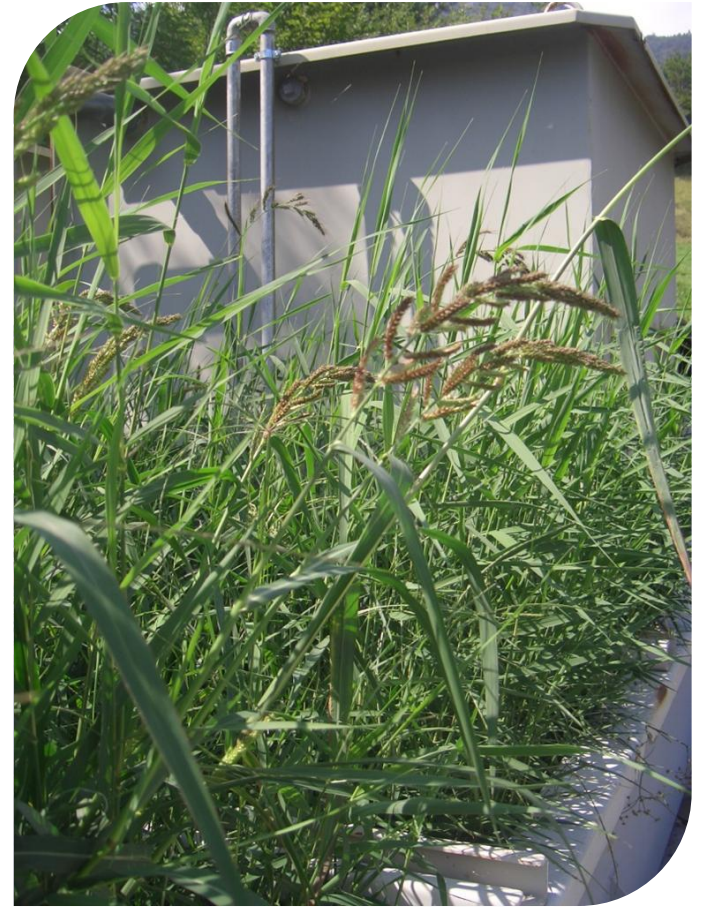
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attention!!!



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